

On the NiMoO_4 oxidative dehydrogenation of propane to propene: some physical correlations with the catalytic activity

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The α - and β -phases of NiMoO_4 have been investigated with different techniques (X-ray diffraction, electrical conductivity, IR spectroscopy) in order to tentatively rationalise the different catalytic activities observed in the oxidative dehydrogenation of propane to propene. XRD analyses have shown that at 595 °C, the β -phase is already present but a temperature of ~ 700 °C is required to obtain a full conversion into a pure β -phase. Electrical conductivity showed the presence of anionic vacancies. It is proposed that propene is formed by the reaction of propane with surface O^{2-} anions. The β -phase is almost twice more selective in propene formation than the α -phase for comparable conversion at identical temperatures. This could derive from different oxygen environments on the active catalytic site.

Keywords: Propane dehydrogenation; nickel molybdate; NiMoO_4 propene formation

1. Introduction

The selective oxidations of lower alkanes are becoming increasingly important both in fundamental and in industrial chemistry. Most of the work published up to now on partial oxidation using gaseous oxygen as an oxidant refers to the oxidation of butane since its total oxidation to maleic anhydride is the only process which is highly selective and operative [1]. For propane dehydrogenation, typical oxidation catalysts are, among others, bismuth, cobalt and nickel molybdates [2–4]. The catalytic properties of these molybdates are closely

related to their structure which depends on the method of preparation and on the thermal treatment.

The preliminary activation of the C-H bond may involve different possibilities which are respectively:

- hydride abstraction [5]
- participation of lattice oxygen [6]
- heterolytic or homolytic bond dissociation [7]
- concerted mechanism [8].

In the present study, we intend to further elucidate the properties of the 2 different phases in the Ni-Mo-O system which, according to its chemical and phase composition, possesses different activities in the oxidative dehydrogenation of propane to propene [4].

2. Experimental

It is known from the literature that NiMoO₄ may exist in three different structures. The two phases which are stable at atmospheric pressure are called hereafter α - and β -phases.

The primary difference between these phases is the co-ordination of molybdenum: octahedral in the α -phase and tetrahedral in the β -phase. It is also known that the β -phase of NiMoO₄, unlike the isotypic phase of CoMoO₄, cannot be quenched at ambient temperature.

1. *Catalysts preparation:* a 0.25 M solution of Ni(NO₃)₂ · 6 H₂O (pH 4.7) and an equal amount of 0.25 M solution of H₂MoO₄ · H₂O in aqueous ammonia (pH 5.6) were mixed at 85 °C. The precipitation was allowed until pH 4.9. The precipitate was filtered at 85 °C and dried at 110 °C for 4 hrs. [9,10].

The α -phase has been obtained by heating the precursor at 550 °C for two hours under normal atmosphere. The purity of the prepared α -NiMoO₄ was checked by Raman spectroscopy to verify the absence of MoO₃.

The surface areas were measured using the BET method. The value of the specific surface area of the α -phase is equal to 40 m²/g. Since the β -phase cannot be quenched at room temperature, its surface area cannot be measured and is assumed to be equal to that of the α -phase reobtained after cooling down of the β -phase at room temperature [9].

2. *High temperature X-rays diffraction experiments:* high temperature X-rays diffraction experiments have been carried out in air using a Siemens D501 diffractometer. A linear counter ELPHYSE associated to a 4096 channel card connected to a PDP 11/24 computer allowed fast data acquisition. Such an equipment is necessary to follow kinetics of reactions in satisfactory conditions [11].

A series of X-ray experiments has been performed to define the exact conditions of formation of β -nickel molybdate. Within the frame of these conditions electrical conductivity measurements and catalytic tests have been carried out on pure α - or β -nickel molybdate.

3. *Electrical conductivity measurements*: they were carried out in a cell of the static type described in ref. [12]. The catalysts were slightly compressed between two platinum electrodes ($P \sim 10^5$ Pa), thus enabling good contacts between particles without modifying the texture.

4. *Infrared spectroscopy*: the spectra (KBr) were recorded using an FT-IR 1720 spectrometer (Perkin-Elmer).

5. *Catalytic tests*: they were carried out as already reported [4]. It should be emphasized that the catalytic tests on the β - NiMoO_4 phase have been carried out first by heating α - NiMoO_4 catalysts at 700°C in oxygen flow for 15 min in order to complete the $\alpha \rightarrow \beta$ transition and then by cooling to the predetermined reaction temperature ($T > 300^\circ\text{C}$) at which no $\beta \rightarrow \alpha$ phase transition occurs [9].

3. Results and discussion

X-RAYS DIFFRACTION EXPERIMENTS

Stoichiometric α - NiMoO_4 has been heated under atmospheric conditions at a rate of $20^\circ\text{C min}^{-1}$ from the room temperature to a temperature T_{w_1} . After one minute, a diffractogram was acquired in four minutes and saved. Then the sample was heated again at the same rate up to a new value T_{w_2} , and studied in the same condition. X-ray diffractions of samples heated at T_{w_i} equal to 595, 620, 640, 665, 675, 695 $^\circ\text{C}$ have been analyzed (fig. 1). Under those dynamic conditions, it is clear that the phase β is already present at 595 $^\circ\text{C}$, but the phase α has not fully disappeared at 695 $^\circ\text{C}$ after 3 minutes. So kinetics of the transformations are to be studied.

The conversion degree λ of the reaction $\alpha \rightarrow \beta$ has been followed under isothermal conditions at 625, 640 and 675 $^\circ\text{C}$. An estimate of this degree was given by the ratio of the intensity of peak of the phase β ($d = 3.34 \text{ \AA}$) during the experience to the same intensity obtained after a treatment at 760 $^\circ\text{C}$ during 5 min performed once the experiment is finished, and a return to the conditions of the experiment. At 760 $^\circ\text{C}$, the phase β is always pure, and the return to the temperature at which the experience was done allows us to avoid corrections of the Debye factor. The reaction is very sensitive to the temperature (fig. 2). The

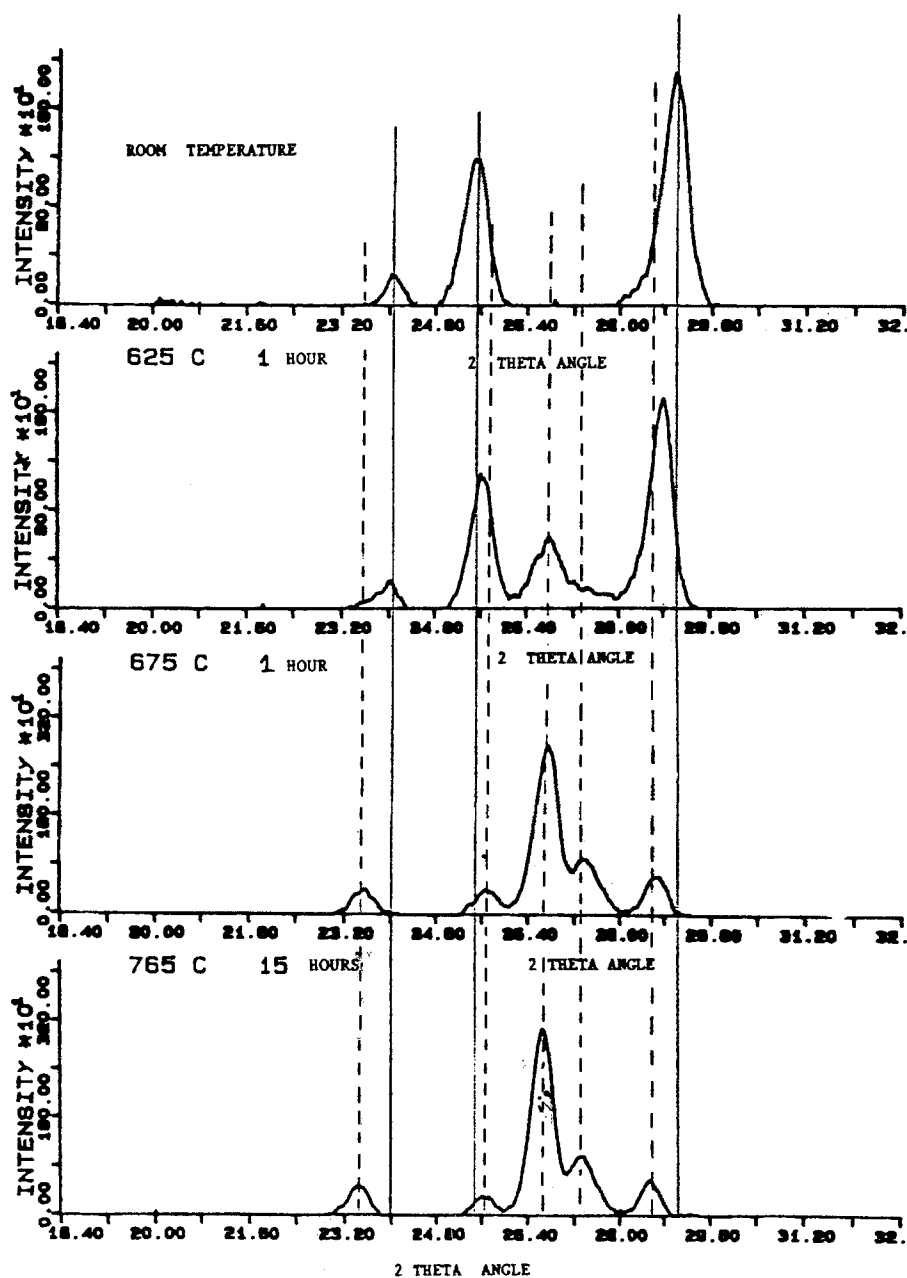


Fig. 1. Diffraction traces of stoichiometric NiMoO_4 . Solid line: α -phase (refs. [18] and [19]); dashed line: β -phase (ref. [19]).

rate is very high just in the beginning of the isotherm, but the yield of reaction presents a very small variation after one hour, and it is strongly related to temperature (625, 675 °C).

ELECTRICAL CONDUCTIVITY MEASUREMENTS

α-phase

The electrical conductivity σ of the phase α was measured as a function of temperature ($440 \leq T \leq 500^\circ\text{C}$) (fig. 3) and oxygen pressure ($1.3 \leq P_{\text{O}_2} \leq 52.6$ kPa) (fig. 4). The conductivity varied according to the experimental law:

$$\sigma = \sigma_0 \cdot \exp(-\Delta H_a/RT) \cdot P_{\text{O}_2}^{-1/n} \quad (1)$$

with an enthalpy of conduction ΔH_a equal to $133,8 \text{ kJ} \cdot \text{mol}^{-1}$ and $n \approx 5.7$.

The value of the exponent is close to the integer 6. This means that the main surface defects are compatible with the model of doubly ionized anionic vacancies $V_{\text{O}}^{\times\cdot}$, which are in equilibrium with oxygen according to the equation:



As a consequence, the labile oxygen species on $\alpha\text{-NiMoO}_4$ in equilibrium with the gas phase are normal oxygen anions located on the surface O_0^{\times} . With respect to the results obtained with $\alpha\text{-NiMoO}_4$, they can constitute oxygen active species in the oxidative dehydrogenation of propane to propene.

Their regeneration would consist in the spontaneous reoxidation of the surface by gaseous O_2 (eq. (2)) according to a Mars and Van Krevelen mechanism.

β-phase

Conductivity measurements were performed on $\beta\text{-NiMoO}_4$ obtained after heating the α -phase in the conductivity cell at 700°C during 900 s and cooling at the desired temperature chosen in the range $440\text{--}500^\circ\text{C}$. As shown in figs. 3

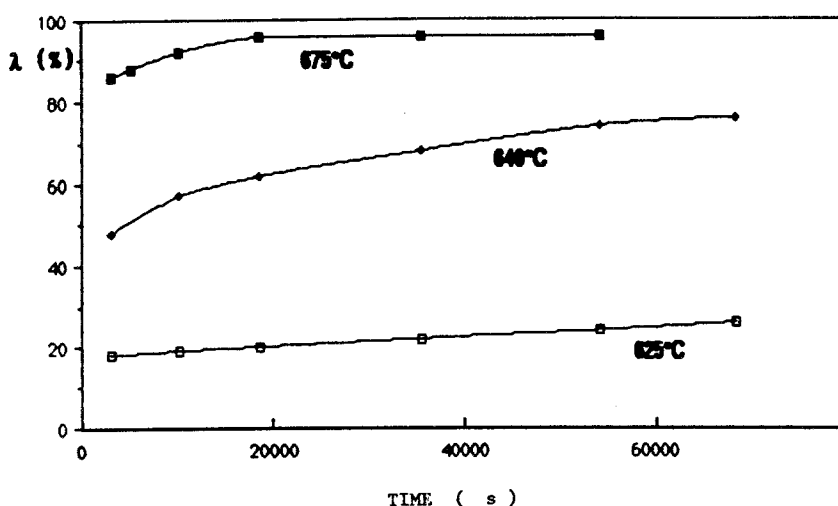


Fig. 2. Kinetics of the transformation $\alpha \rightarrow \beta\text{-NiMoO}_4$ followed by X-ray diffraction analysis (conversion λ (in %) as a function of time).

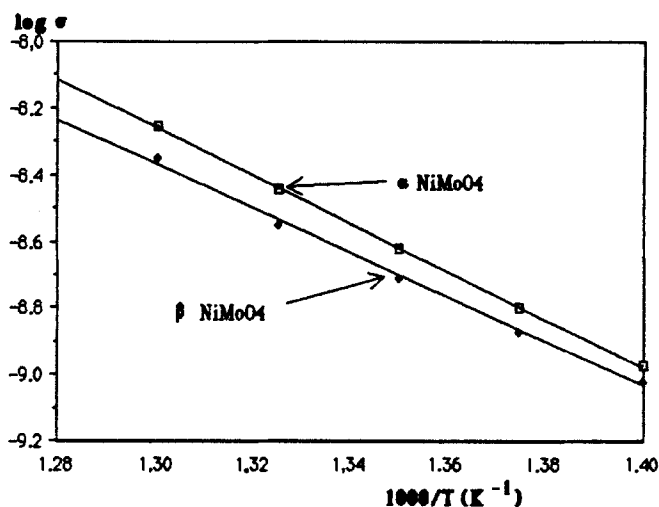


Fig. 3. Electrical conductivity variations as a function of temperature (Arrhenius plot).

and 4, the conductivity of the β -phase follows the same laws as the α -phase for oxygen pressure $P_{O_2} \geq 19.7$ kPa. The value of ΔH_a is equal to 125.4 kJ and that of n close to 4. So, it can be concluded that the major defects in β -NiMoO₄ are anionic oxygen vacancies, singly ionized. Both α - and β -NiMoO₄ exhibit an n-type semiconduction and for the β -phase:



INFRARED SPECTROSCOPY

It has been reported by Chaar and his colleagues that the V₂O₅/MgO catalyst system shows appreciable activity and selectivity for the oxidative dehydrogenation of propane [13] and butane [14]. This has been attributed to the absence of V=O bonds found in pure V₂O₅ which cause the formation of oxygen containing products. Recent results [15] seem to confirm that selective oxidation of ethane and propane over alkali and alkaline earth orthovanadates, due to the absence of V=O species, mainly depends on the strength of the V-O-V bond.

Referring now to the MoO₃/NiO system we are not aware of specific correlations between infrared absorptions and catalytic activities in the oxidative dehydrogenation of alkanes. At this regard some references can be cited with respect to pure MoO₃ and MoO₃/CoO which is characterized by phase-transition effects similar to those reported for MoO₃/NiO. As for MoO₃, the band at 980 cm⁻¹ is normally attributed to the Mo=O bond while the bands at 870 and 812 cm⁻¹ are attributed to Mo-O- bonds. Any shift of the band having the nature of a double bond to lower frequencies implies a decrease in the

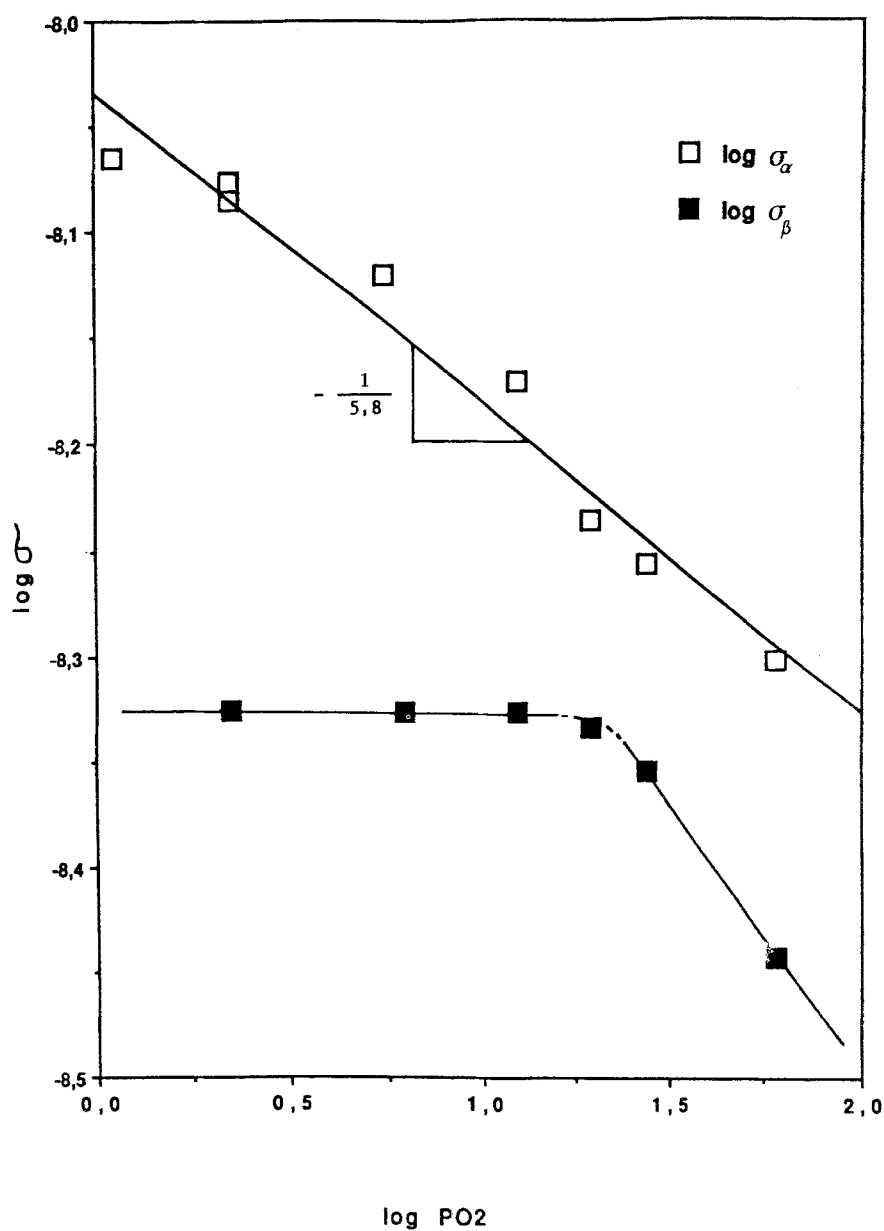


Fig. 4. Variations of the electrical conductivity as a function of oxygen pressure (in kPa) ($T = 500^\circ \text{C}$).

characteristics of double bond and an increase in the labilization of the bond itself [16].

Similar shifts occur with CoMoO_4 . Indeed with green CoMoO_4 there is a strong absorption band at 945 cm^{-1} which is typical of the octahedral configuration of Mo. For violet CoMoO_4 , based on ATR techniques and assuming that

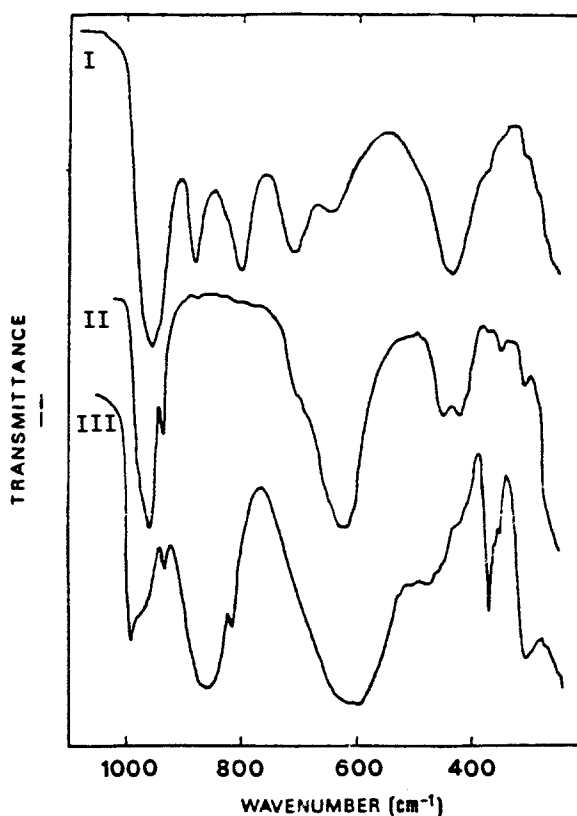


Fig. 5. IR spectra of α - and β - NiMoO_4 phases.

the observed differences of band intensities cannot be justified by different energy dispersions between IR and ATR techniques, the shift is even greater (at 930 cm^{-1}) while two novel absorptions at 840 and 780 cm^{-1} become evident. A tetrahedral coordination is assumed for Mo together with the possibility of absorption of the second metal [17]. Significantly, when considering the results obtained in the oxidative dehydrogenation of 1-butene, green α - CoMoO_4 gives only traces of 1,3-butadiene, whereas the violet β -phase gives small but significant quantities of the same products.

Pure β - NiMoO_4 cannot be obtained at room temperature as β - CoMoO_4 because it is not metastable. Fig. 5 typically refers to β - NiMoO_4 solid solution stabilized [10] with excess NiO (I), pure α - NiMoO_4 (II), $\text{NiMoO}_4 \cdot 5\text{ MoO}_3$ (III). Stabilized β - NiMoO_4 (I) exhibits at ca 950 cm^{-1} an absorption band and two novel absorption bands at ca. 880 – 800 cm^{-1} which are characteristic of β - NiMoO_4 .

It may be seen that when passing from (III) to (II) to (I) the striking differences observed may be rationalized in view of the discussion reported above. Considering the different catalytic activities of α - and β - NiMoO_4 re-

Table 1

Catalytic activities of both NiMoO₄ phases at various temperatures

Catalyst NiMoO ₄ phase	Tempera- ture (°C)	Conver- sion (%)	Activity in C ₃ H ₆ (mmol/h)	Intrinsic activity in C ₃ H ₆ (mmol/h/m ²)
α	500	9.6	4.7	0.23
	530	15.2	7.0	0.35
	560	24.8	9.2	0.46
β	500	7.2	5.6	0.75
	530	12.5	9.2	1.23
	560	20.85	13.2	1.76

Feed: 15% C₃H₈ + 15% O₂ in N₂.

Total feed 15 l/h for 500 mg of catalyst.

ported in this work, for the latter catalyst we postulate a multifunctional (Ni-O-Mo linkages) nature of the active site for propane oxidative dehydrogenation.

Catalytic results

Both α - and β -phases characterized above were tested in the oxidative dehydrogenation (OXD) of propane into propene at different temperatures. All the catalytic results (activity, conversion and selectivities) are listed in tables 1 and 2. It appears that the overall conversion is of the same order for both phases. However, the selectivity in propene formation for the β -phase is almost twice as big as that of the α -phase, propene remaining the major reaction product in the two cases. Moreover, the intrinsic activity (in mol/h/m²) of the β -phase is ca. 3.5 bigger than that of the α -phase. Electrical conductivity measurements versus P_{O_2} have shown the presence of anionic vacancies in the surface lattice of nickel molybdates. The formation of propene can proceed via

Table 2

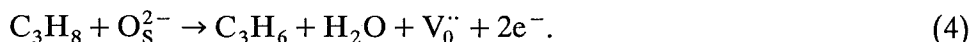
Selectivities in various oxidation products at various temperatures

Catalyst NiMoO ₄ phase	Tempera- ture (°C)	Conver- sion (%)	Selectivities (%)					
			CO	CO ₂	C ₂ H ₄	C ₃ H ₆	CH ₃ CHO	CH ₂ CHCHO
α	500	9.6	23.0	21.4	2.0	49.0	0.6	4.0
	530	15.2	27.0	21.0	2.0	46.2	0.5	3.0
	560	24.8	32.2	24.6	2.0	37.5	0.2	3.0
β	500	7.2	10.3	8.0	0.7	78.1	0.3	2.5
	530	12.5	12.0	10.1	1.0	73.0	0.7	3.0
	560	20.85	18.0	14.0	1.3	63.1	0.3	3.5

Feed: 15% C₃H₈ + 15% O₂ in N₂.

Total feed 15 l/h for 500 mg of catalyst.

the formation of such vacancies by reaction with O²⁻ surface anions according to the reaction:



The difference in propene selectivities can be attributed to a difference in reactivity of lattice O²⁻ anions present at the surface of both phases; this may arise from different oxygen environments on the active catalytic site (see infrared evidences).

4. Conclusion

It has been demonstrated by different techniques (X-ray analysis, electrical conductivity, IR spectroscopy) that the two phases of NiMoO₄ (α and β) are significantly different. The same phases differ also in terms of catalytic activity. The β -phase has an intrinsic activity equal to about 3.5 times that of the α -phase, whereas the selectivity in propene is correspondingly twice as big.

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References

- [1] K.B. Hodnett, Catal. Rev. Sci. Eng. 27 (1985) 373.
- [2] G. Minow, K. Schnabel and G. Ohlmann, React. Kinet. Catal. Lett. 22 (1983) 399.
- [3] Hardman, F. Harley, U.S. Patent 4255284 Mar. 10, 1981 to Standard Oil Company.
- [4] C. Mazzocchia, E. Tempesti and C. Aboumrar, Fr. Patent 89-00522 18 Jan, 1989 to Norsolor.
- [5] H. Hattori, O. Takahashi, M. Takagi and K. Tanabe, J. Catal. 68 (1980) 132.
- [6] M.B. Ward, M.J. Lin and J.H. Lunsford, J. Catal. 50 (1977) 306.
- [7] K.T. Nguyen and H.H. Kung, J. Catal. 122 (1990) 415.
- [8] G. Centi and F. Trifiro, *Symp. on Hydroc. Oxidation*, Amer. Chem. Soc., New Orleans Meeting, August 30–September 4 (1987) 754.
- [9] C. Mazzocchia, F. Di Renzo, P. Centola, R. Del Rosso, in: *Chemistry and Uses of Molybdenum*, eds. H.F. Barry and P.C.H. Mitchell (Golden, CO., 1983) p.406.
- [10] C. Mazzocchia, F. Di Renzo, C. Aboumrar and G. Thomas, Solid State Ionics 32/33 (1989) 228.
- [11] G. Thomas, M. Millet and A. Sebaoun, Thermochemica Acta 85 (1985) 135.
- [12] J.M. Herrmann, in: *Les techniques physiques d'étude des Catalyseurs*, eds. J. Védrine and B. Imelik (Editions Technip., Paris, 1988) p.753.

- [13] M.A. Chaar, D. Patel and H.H. Kung, *J. Catal.* 109 (1988) 463.
- [14] M. Lee Fu, U.S. Patent 44607129, Philips Petroleum Co., 1986.
- [15] K. Seshan, H.M. Swaan, R.H.H. Smits, J.V. Van Ommen and J.R.H. Ross, *New Developments in Selective Oxidation*, Preprints, paper H.2, Rimini, 1989.
- [16] F. Trifiro, P. Centola, I. Pasquon and P. Jiru, *Proc. 4th Int. Congress on Catalysis*, Moscow 1968, Paper 18.
- [17] F. Trifiro, G. Caputo and P.L. Villa, *Journal of the Less-Common Metals* 36 (1974) 305.
- [18] Powder diffraction file, International Center for Diffraction Data, Swarthmore (USA), 1989, p. 332, file n° 33-948.
- [19] C. Mazzocchia, F. DiRenzo, R. Anouchinsky and G. Thomas, *Proc. Congr. Phys. Chem.*, Societa di Fisica Chimica Italiana, Siena, 1986.